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# Non-isothermal studies for the decomposition course of  $CdC_2O_4$ – $ZnC_2O_4$  mixture in air

M.A. Gabal∗

*Chemistry Department, Faculty of Science, Benha University, Benha, Egypt*

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## **Abstract**

The thermal decomposition of cadmium–zinc oxalate (1:1 mol ratios) mixture in air was investigated by non-isothermal thermogravimetric analysis. Intermediates and the final products were characterized by X-ray diffraction and scanning electron microscopy techniques. TG showed that the mixture dehydrated in two steps and decomposed exothermically to CdO–ZnO mixture at 390 ◦C in a further two steps. The observed increase in the intensity of the X-ray diffraction lines by raising the calcination temperature from 400 to 800 ◦C is attributed to the grain growth of CdO–ZnO mixture as revealed from SEM experiments. The kinetics of the oxalate decomposition steps was performed using the various reaction interface models and differential techniques of computational analysis of non-isothermal data. The activation parameters, calculated using the integral composite method, showed that the reactions were best described by the random nucleation model characteristic of solid state nucleation growth mechanism. The results of activation parameters for the different decomposition steps are compared and discussed. © 2003 Elsevier B.V. All rights reserved.

*Keywords:* CdC2O4; ZnC2O4; DTA-TG; SEM; Kinetics; Oxalates

## **1. Introduction**

The thermal decomposition of metal oxalates is occasionally adopted as a means of preparing metals or metal oxides possessing pores, lattice imperfections and other characteristics necessary for their function as reactive solids [1]. Much researches [2] has been done on the structure, properties and thermal decomposition behaviors of metal oxalates and a considerable amount of information on the kinetics of the thermal dehydration and decompositio[n of](#page-7-0) them have been r[epor](#page-7-0)ted [3]. The combination of transition metal oxides may results in the modification of their thermal behavior, geometric structure and electronic properties that lead to changes in their catalytic functions [4]. Thus, the different synthesis [me](#page-7-0)thods of the mixed metal oxides and their characterization have been the subject of many numerous investigations.

The physico-chemical properties as well as the reactivity towards the [redu](#page-7-0)ction with hydrogen of  $CuO-Cr<sub>2</sub>O<sub>3</sub>$ mixed oxides prepared by the thermal decomposition of basic metal carbonate precipitates have been investigated by means of various techniques [5]. Mucka and Pavek [6] tested the catalytic activity of the two-component oxide catalyst CdO–ZnO prepared from the thermal decomposition of nitrate precursors by means of hydrogen peroxide decomposition in a water [solut](#page-7-0)ion. Giullermo e[t al.](#page-7-0) [7] studied the electrical and optical properties of a mixed thin film oxides of cadmium and zinc with different compositions prepared by spray pyrolysis deposition on a glass substrates.

The mixed metal oxalates [\[8\];](#page-7-0) FeCu(OX) $_2$ ·3H $_2$ O,  $CoCu(OX)_2.3H_2O$  and  $NiCu(OX)_2.3.5H_2O (OX = C_2O_4^-)$ have been prepared by coprecipitation technique and their thermal behaviors in nitrogen and oxygen have been examined using thermogravi[metr](#page-7-0)y (TG), thermomagnetometry (TM), differential scanning calorimetry (DSC) and evolved gas analysis (EGA). In a previous paper [9], the thermal decomposition processes taking place in the solid state mixed oxalates of  $(CuC_2O_4-ZnC_2O_4.2H_2O, 1:1 \text{ mol ratios})$  was studied in air using differential thermal analysis thermogravimetry (DTA-TG), X-ray [diff](#page-7-0)raction (XRD) and scanning electron microscopy (SEM) techniques. The kinetics of the oxalate decomposition steps were performed under non-isothermal conditions using different integral methods of analysis of dynamic data.

<sup>∗</sup> Present address: Institute of Mechanical Engineering and Mechanics (IMVM), University of Karlsruhe, Geb. 30.70, Kaiser Street 12, Karlsruhe 76128, Germany. Tel.: +49-201-01048600; fax: +49-201-3222578.

*E-mail address:* mgabalabdo@yahoo.com (M.A. Gabal).

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The dynamic thermogravimetric analysis has been widely used as a tool to investigate the sample composition, the thermal stability as well as the kinetic data relating the chemical changes occur on heating [10]. In the present study, the thermogravimetry was used to study the kinetics of the thermal decomposition of  $CdC_2O_4.3H_2O-ZnC_2O_4.2H_2O$  (1:1 mol ratios) mixture in air. The kinetic analysis of data were performed and [consid](#page-7-0)ered with reference to the various theoretical model equations and integral methods of dynamic data analysis. The thermal decomposition course of the mixture was characterized using DTA-TG, XRD and SEM techniques.

## **2. Experimental**

#### *2.1. Materials*

Pure metal oxalates were prepared by precipitation from aqueous solutions of analytical reagents  $3C dSO_4.8H_2O$ or  $ZnCl_2·2H_2O$  on the addition of hot oxalic acid solution. The physical mixture  $CdC_2O_4.3H_2O-ZnC_2O_4.2H_2O$ (1:1 mol ratios) was prepared by the impregnation method. The appropriate mole ratios of the individual metal oxalates were grounded together in a porcelain mortar. During the vigorous stirring, drops of bi-distilled water were added to assure complete homogeneity. The wet oxalate mixture was dried at  $60^{\circ}$ C for about 2 h.

On the basis of the thermal analysis results, the cal[cina](#page-7-0)tion products of the mixture were obtained by heating the mixture in static air at 340 ◦C for 15 min, at 400 ◦C for 1 h or at  $800\degree$ C for 2 h. Prior to the analysis, the calcinations products were kept dry over anhydrous calcium chloride in a desiccator.

## *2.2. Apparatus*

Thermal analysis experiments including thermogravimetry (TG), differential thermogravimetry (DTG) and differential thermal analysis (DTA) were carried out using a Shimadzu DT-40 thermal analyzer. All the experiments were carried out in a dynamic  $(30 \text{ ml min}^{-1})$  atmosphere of air in order to prevent the accumulation of the gaseous products. Sample weights in the Pt-cell of 8–10 mg, were used in these experiments, to ensure linear heating rates and accurate temperature measurements. Highly sintered  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> powder (Shimadzu) was used as the reference material for the DTA measurements. In the dynamic studies, the temperature was raised up to 400 °C at heating rates of 1, 2, 3 and  $5^{\circ}$ C min<sup>-1</sup>.

X-ray powder diffraction analysis of the solid decomposition products was carried out using a Philips PW 1710 diffractometer at ambient temperature using Ni-filtered Cu K $\alpha$  radiation ( $\lambda = 1.5406$  Å). For the identification purpose, the relative intensities  $(I/I_0)$  and the *d*-spacing  $(\AA)$  were compared with standard diffraction patterns of the ASTM powder diffraction files [11].

SEM is performed using Jeol T 300 (Japan) scanning electron microscope operated at 15 keV. Mixtures were mounted separately on aluminum substrates evacuated to  $10^{-3}$  Torr and precoated (20 and 5 min for each side of the four sides) in a sputter-coater with a thin uniform gold/palladium film to minimize charging in the electron beam. The applied voltage is 1.2–1.6 kV.

#### *2.3. Data analysis*

Kinetics parameters such as the activation energy (*E*) and the frequency factor (*A*) were calculated from the dynamic TG curves assuming the Diefallah's composite integral method based either on the modified Coats–Redfern equation (composite method I) or on Doyle's equation (composite method II) [9,12,13]. In the composite method I, the modified Coats–Redfern equation was rewritten in the form:

$$
\ln\left[\frac{\beta g(\alpha)}{T^2}\right] = \ln\left(\frac{AR}{E}\right) - \frac{E}{RT}
$$
 (1)

where *A* is the frequency factor, *E* the energy of activation and  $g(\alpha)$  the kinetic model function calculated for the fraction reacted  $(α)$  at temperature *T* and heating rate  $β$ . Table 1 shows the different kinetic model functions used in this work [9]. In the composite method II, Doyle's equation has been rewritten in the form:

$$
\log g(\alpha)\beta = \left[\log \frac{AE}{R} - 2.315\right] - 0.4567 \frac{E}{RT} \tag{2}
$$

hence, the dependence of  $\ln[\beta g(\alpha)/T^2]$  or  $\log[g(\alpha)\beta]$ , calculated for the different  $α$ -values at their respective  $β$ -values on 1/*T* must give rise to a single master straight line for the correct form of  $g(\alpha)$ . Generally, the results always show that [9,12,13] both the composite methods of analysis gave equivalent curves and nearly identical values for the calculated activation parameters. The composite method also

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Kinetic equations examined in this work



<span id="page-2-0"></span>involves a model-fitting kinetic approach, since it does not assume a particular reaction model, but it allows the choice of the kinetic mechanism which best fits the data and gives the highest correlation coefficient.

The activation parameters were then calculated using two other integral methods: the Coats–Redfern method [14] and the Ozawa method [15] assuming the best fit kinetic model obtained from the composite method. The obtained activation parameters were then compared with those obtained according to the composite method and di[scusse](#page-7-0)d.

## **3. Results and discussion**

## *3.1. Thermal analysis*

Fig. 1 shows the characteristic features of heating  $CdC<sub>2</sub>O<sub>4</sub>·3H<sub>2</sub>O-ZnC<sub>2</sub>O<sub>4</sub>·2H<sub>2</sub>O$  (1:1 mol ratio) mixture in air atmosphere from the ambient temperature to 400 ◦C. It shows the DTA, TG and DTG curves that were measured at 5 ◦C min−1. The TG curve shows four mass loss steps. The first two steps occurring at  $65-140\degree$ C and are accompanied by 11.5 and 8.5% mass loss, i.e. a total mass loss of 20.0% which is attributed to the complete dehydration of the mixture with the formation of anhydrous mixture (theoretical mass loss, 20.3%). From the theoretical mass loss, the first step can be attributed to the dehydration of  $CdC<sub>2</sub>O<sub>4</sub>·3H<sub>2</sub>O$ and the second one is attributed to the dehydration of  $ZnC_2O_4.2H_2O$ . Nagase et al. [16] showed that the dehydration temperature is a function of the size of metal ion and that it increases with the decrease in the radius of the metal ion. The ionic radius [17] of Cd(II) and Zn(II) ions are 0.97 and 0.76 Å, r[espec](#page-7-0)tively. Thus,  $CdC<sub>2</sub>O<sub>4</sub>·3H<sub>2</sub>O$  must be dehydrated at lower temperature than  $ZnC_2O_4.2H_2O$ . The anhydrous mixture is thermally stable up to  $290\degree\text{C}$ after which [a two](#page-7-0) consecutive mass loss steps were occurred in the temperature ranges 290–340 and 340–380 ◦C.

These steps were associated by 16.5 and 16.7% mass loss due to the decomposition of  $CdC_2O_4$  and  $ZnC_2O_4$  in their mixture to CdO and ZnO (theoretical mass loss in both the steps is 16.2%), respectively. The total mass loss after complete decomposition was calculated to be 42.4% of the molecular mass of the reactants. From the above data, the temperatures equivalent to the theoretical mass losses can then be considered as the minimum temperatures which can be selected for the calcination process.

The DTG curve displays four broad peaks, which are closely correspond to the weight changes observed on the TG curves, with maximum rates of loss at about 92, 136, 326, and 366 ◦C, respectively.

The DTA curve reveals also four broad peaks maximized at 90 °C (endo), 132 °C (endo), 330 °C (exo) and 365 °C (exo), respectively. The two endothermic peaks are attributed to dehydration. Dollimore et al. [18,19] studied the thermal decomposition of  $ZnC_2O_4$  and  $CdC_2O_4$  in air and nitrogen atmospheres and found that the end product in case of  $ZnC_2O_4$  to be  $ZnO$  in both atmospheres whereas in case of  $CdC<sub>2</sub>O<sub>4</sub>$  the end pro[duct in ni](#page-7-0)trogen is Cd metal and in air is CdO. Thus the exothermic nature of the DTA peaks accompanying the first oxalate decomposition process (i.e. the decomposition process of  $CdC<sub>2</sub>O<sub>4</sub>$  is attributed to the air oxidation of Cd metal to CdO, whereas the exothermic behavior of the second oxalate decomposition process (i.e. the decomposition process of  $ZnC_2O_4$ ) is due to the catalytic oxidation reaction of CO as it forms to  $CO<sub>2</sub>$  on the surface of ZnO product.

The above thermal analysis results indicate that,  $CdC_2O_4.3H_2O$  and  $ZnC_2O_4.2H_2O$  decomposed in their mixture similarly to their individual metal oxalates [18,19]. This behavior is ascribed to the absence of any solid solution between the two metal oxalates and that each one behaves as it is present alone in the mixture. A similar behavior was obtained for the thermal deco[mposition](#page-7-0) reaction of  $CuC<sub>2</sub>O<sub>4</sub> - ZnC<sub>2</sub>O<sub>4</sub> \cdot 2H<sub>2</sub>O mixture [9].$ 



Fig. 1. DTA-TG curves of CdC<sub>2</sub>O<sub>4</sub>·3H<sub>2</sub>O–ZnC<sub>2</sub>O<sub>4</sub>·2H<sub>2</sub>O (1:1 mol ratios) mixture in air at heating rate of 5 °C min<sup>-1</sup>.



Fig. 2. Characteristic parts of XRD patterns of CdC2O4·3H2O–ZnC2O4·2H2O (1:1 mol ratios) mixture calcined at different temperatures. Mixture calcined at (a)  $400\degree C$  and (b)  $800\degree C$ .

#### *3.2. X-ray diffraction*

The XRD diffraction pattern of the initial mixture matched the standard data compiled in the JCPDS data [11] no. 14–750 and 25–1029 for individual  $CdC_2O_4.3H_2O$ and  $ZnC_2O_4.2H_2O$ , respectively. The XRD pattern of the decomposition products at 340 ◦C reveals the characteristic XRD lines for CdO (JCPDS no. 5–640). The presence of some XRD lines characteristic of hydrated zinc oxalate may be attributed to the hydration of the anhydrous zinc oxalate [20] formed at this decomposition stage.

Fig. 2 shows the characteristic X-ray diffraction patterns at ambient temperature for mixture calcined at 400 and 800 ◦C for the mixture calcined at  $400\degree C$ , the presence of the individual characteristic XRD lines (Fig. 2a) of both CdO and ZnO (JCPDS no. 5–640 and 21–1486, respectively) indicate the complete decomposition of the mixture without formation of any solid solution. The broadening of the XRD lines is attributed to the weak crystallinity of the decomposition products. Generally no solid solution was detected between the two metal oxides even by raising the calcination temperature to  $800\degree$ C. This was achieved by comparing the XRD patterns of the mixture calcined at  $400\degree C$  with that calcined at  $800\degree$ C (Fig. 2a and b), where the only difference is the increase in the intensities of the XRD lines. This behavior is ascribed to the sintering process.  $(ZnO)_x(CdO)_{1-x}$ thin films of  $(ZnO)_x(CdO)_{1-x}$  prepared by spray pyrolysis on a glass substrates [7] showed the presence of CdO XRD pattern for low zinc concentrations and a mixture of CdO (cubic) and ZnO (hexagonal) phases for the higher concentrations. The XRD pattern of this system shows also an increase in [the c](#page-7-0)rystallite sizes with annealing. A similar trend was also obtained for CuO–ZnO mixture prepared from  $CuC_2O_4$ - $ZnC_2O_4$  $·2H_2O$  (1:1 mol ratios) mixture [9].

#### *3.3. Electron microscopy*

Samples of the initial mixture as well [as](#page-7-0) [int](#page-7-0)ermediate decomposition products formed at different temperatures were examined using scanning electron microscopy to characterize the textural changes that occurring during the decomposition reaction of the mixture. The parent mixture has very small individual crystallites  $(<0.5 \mu m$ ) which make the textural features resolution difficult. The change in the particle size and shape throughout the decomposition process is shown in Fig. 3. The scanning electron micrograph of the mixture calcined at  $340\degree$ C (Fig. 3a) shows, in addition to the large irregularly shaped crystals of different sizes, aggregates of approximately spherical particles showing n[o regula](#page-4-0)r or characteristic crystalline structures.

<span id="page-4-0"></span>

Fig. 3. Scanning electron micrograph showing the changes in texture and morphology that accompany the thermal decomposition of  $CdC<sub>2</sub>O<sub>4</sub>·3H<sub>2</sub>O-ZnC<sub>2</sub>O<sub>4</sub>·2H<sub>2</sub>O$  (1:1 mol ratios) mixture in air. Mixture calcined at (a)  $340^{\circ}$ C, (b)  $400^{\circ}$ C and (c)  $800^{\circ}$ C (scale bar  $10 \mu$ m).

At this calcinations temperature the DTA-TG results show only the decomposition of  $CdC<sub>2</sub>O<sub>4</sub>$  content into CdO while ZnC2O4 content remains undecomposed. The large crystals can be assigned to the undecomposed zinc oxalate while the particles aggregates can be ascribed to the decomposition of cadmium oxalate content into small and fine granules with roughening of the crystal surfaces. At  $400^{\circ}$ C, the zinc oxalate content was decomposed, so, the micrograph obtained for the mixture at this temperature (Fig. 3b) shows the complete breaking into fine granules, with superficial roughening of the crystal edges, which provide evidence that the oxides formed at this stage are microcrystalline as previously suggested by XRD experiments. In the mixture calcined at  $800\,^{\circ}\text{C}$ , these fine granules were coalesced into large aggregates of cubic crystals of different sizes (Fig. 3c).

## *3.4. Kinetic studies*

The kinetics of the thermal decomposition in air of  $CdC<sub>2</sub>O<sub>4</sub>$  to CdO (step III) and of  $ZnC<sub>2</sub>O<sub>4</sub>$  to ZnO (step IV) in  $CdC_2O_4.3H_2O-ZnC_2O_4.2H_2O$  (1:1 mol ratio) mixture were studied under non-isothermal conditions. Typical plots of weight changes from dynamic measurements at different constant heating rates versus decomposition temperature for these two steps are shown in Fig. 4. Kinetic analysis of data according to the composite method showed that the decomposition steps were best described by Avrami–Erofeev random nucleation equations  $(A_2 \text{ and } A_3)$  characteristic of solid state nucleation [growth](#page-5-0) mechanism, consistent with the textural changes that accompanying the decomposition as revealed by SEM experiments. The phase boundary controlled reaction equations ( $R_2$  and  $R_3$ ), in which an interface moves at constant velocity and nucleation occurs virtually instantaneously, gave also a satisfactory results. The other model equations give a less satisfactory fit of the data and the exponential law equation  $(E_1)$  gave the least fit. Table 2 lists the values of activation parameters, calculated according to the composite method based on the Doyle's equation (composite II method) assuming different heterogeneous solid state models, for the non-isother[mal decom](#page-5-0)position of  $CdC<sub>2</sub>O<sub>4</sub>$  and  $ZnC<sub>2</sub>O<sub>4</sub>$  in their mixture. Fig. 5 shows the typical results calculated by the composite method on the basis of the Doyle's equation assuming  $A_2$  and  $E_1$  models.

The activation parameters were also calculated on the basis of the Coats–Redfern and [Ozawa](#page-5-0) methods assuming A2 model (as revealed by the composite method). Then the calculation results according to the three computational methods were summarized in Table 3. The listed values for the activation parameters in case of the Coats–Redfern and the Ozawa methods are the average ones calculated at different heating rates ( $\beta$ ) and fractional reaction ( $\alpha$ ) values, respectively.

Approximately constant  $E$  with  $\alpha$  was obtained on plotting the calculated activation energy (*E*), estimated by the Ozawa method, versus the fractional reacted vales  $(\alpha)$  for the two oxalate decomposition reactions (Fig. 6). As a result, this will enhance that the rate-limiting step is a single reaction step [9] in accordance with the single master straight line for all  $(\alpha, \beta, T)$  values obtained at different heating rates estimated by the compo[site met](#page-6-0)hod (Fig. 5).

The results of data analysis using the different computational methods (Table 3) show a good agreement within experimental errors between the values of the calculated activation parameters. The [data also](#page-5-0) shows that, the integral composite method of analysis gave the least standard deviation in [the calcu](#page-6-0)lated experimental parameters. Generally,

<span id="page-5-0"></span>

Fig. 4. Dynamic measurements for the thermal decomposition of CdC<sub>2</sub>O<sub>4</sub>·3H<sub>2</sub>O–ZnC<sub>2</sub>O<sub>4</sub>·2H<sub>2</sub>O (1:1 mol ratios) mixture in air. (a) Decomposition of CdC<sub>2</sub>O<sub>4</sub> to CdO and (b) ZnC<sub>2</sub>O<sub>4</sub> to ZnO. Heating rate: curve A, 1 °C min<sup>-1</sup>; curve B, 2 °C min<sup>-1</sup>; curve C, 3 °C min<sup>-1</sup> and curve D, 5 °C min<sup>-1</sup>.

Table 2 Activation parameters of the non-isothermal decomposition in air of  $CdC_2O_4$  and  $ZnC_2O_4$  in their mixture, calculated according to the composite method II, assuming different kinetic models

Model	Decomposition of $CdC2O4$ (step III)			Decomposition of $ZnC2O4$ (step IV)		
	$E$ (kJ mol <sup>-1</sup> )	$\log A$ (min <sup>-1</sup> )	r	$E$ (kJ mol <sup>-1</sup> )	$\log A$ (min <sup>-1</sup> )	
$D_1$	$355 \pm 21$	$30.8 \pm 2.1$	0.872	$529 \pm 35$	$30.0 \pm 3.4$	0.817
$D_2$	$378 \pm 23$	$32.8 \pm 2.2$	0.873	$562 \pm 44$	$30.0 \pm 3.7$	0.816
$D_3$	$407 + 25$	$35.0 \pm 2.4$	0.872	$604 + 47$	$30.0 \pm 3.9$	0.816
$D_4$	$387 \pm 24$	$33.1 \pm 2.3$	0.873	$575 \pm 45$	$30.0 \pm 3.8$	0.816
$R_2$	$218 \pm 8$	$18.3 \pm 0.7$	0.952	$318 \pm 15$	$25.4 \pm 1.3$	0.961
$R_3$	$225 \pm 8$	$18.8 \pm 0.8$	0.951	$327 \pm 16$	$26.1 \pm 1.4$	0.913
$F_1$	$241 \pm 9$	$20.9 \pm 0.9$	0.946	$357 \pm 18$	$28.5 \pm 1.6$	0.907
A <sub>2</sub>	$142 \pm 2$	$11.9 \pm 0.2$	0.994	$210 \pm 3$	$16.6 \pm 0.2$	0.995
$A_3$	$109 \pm 4$	$8.9 \pm 0.4$	0.855	$163 \pm 3$	$12.7 \pm 0.3$	0.982
$E_1$	$133 \pm 25$	$13.3 \pm 2.3$	0.467	$168 \pm 38$	$15.2 \pm 3.2$	0.402



Fig. 5. Composite analysis of TG data for the non-isothermal decomposition in air of (A) CdC2O4 and (B) ZnC2O4 in their mixture based on Doyle's equation assuming: (1)  $A_2$  model; (2)  $E_1$  model.

<span id="page-6-0"></span>Table 3 Activation parameters of the non-isothermal decomposition in air of  $CdC<sub>2</sub>O<sub>4</sub>$  and  $ZnC<sub>2</sub>O<sub>4</sub>$  in their mixture calculated according to  $A<sub>2</sub>$  model

Method of	Decomposition of		Decomposition of		
analysis	$CdC2O4$ (step III)		$ZnC2O4$ (step IV)		
	E	log A	E	log A	
	$(kJ \text{ mol}^{-1})$	$(min^{-1})$	$(kJ \text{ mol}^{-1})$	$(min^{-1})$	
Composite II	$142 + 2$	$11.9 \pm 0.2$	$210 \pm 3$	$16.6 \pm 0.2$	
Coats-Redfern	$136 \pm 10$	$11.3 \pm 0.7$	$216 \pm 16$	$17.2 + 1.4$	
Ozawa	$153 \pm 4$	$12.9 \pm 0.3$	$198 \pm 5$	$15.6 \pm 0.5$	

on comparing the activation energies obtained in Table 3 for the thermal decomposition of  $CdC_2O_4$  and  $ZnC_2O_4$  in their mixture it is obvious that the activation energy for the thermal decomposition of zinc oxalate is higher (about 30% more) than that needed for the thermal decomposition of cadmium oxalate. In addition, the DTA-TG results (Fi[g.](#page-7-0) [1\)](#page-7-0) shows that the thermal stability of  $CdC<sub>2</sub>O<sub>4</sub>$  is less than that of  $ZnC<sub>2</sub>O<sub>4</sub>$ .

In the oxalates of bivalent metals:

$$
\text{M} \text{O}^{-C=O_{\text{II}}}_{\text{O}_{\text{I}} \text{C}=O_{\text{II}}}
$$

the extent to which the  $M-O<sub>I</sub>$  bond is covalent depend on the electronegativity of the metal. Decomposition will occur when a temperature is reached at which the rupture of the M[–O](#page-2-0)<sub>I</sub> link is possible or at which the rupture of  $C$ –O<sub>I</sub> bond occurs. For these oxalates which produce the metal in nitrogen the decomposition temperature represents the temperature at which the  $M-O<sub>I</sub>$  link ruptured and will depend critically on the size and charge of the metal ion. Whereas in these decompositions where the oxide is produced in nitrogen the decomposition temperatures represents the energy required to break the  $C-O<sub>I</sub>$  bond and this will depend less critically on the nature of cation. If the reaction proceeds by the rupture of the  $C-O<sub>I</sub>$  bond, this would be followed by the rupture of the second  $M-O<sub>I</sub>$  bond because the inability of the metal to accommodate two oxygen atoms.

The thermal decomposition of  $ZnC_2O_4$  in air or nitrogen atmospheres results in the production of ZnO, whereas the thermal decomposition of  $CdC<sub>2</sub>O<sub>4</sub>$  in nitrogen produces Cd metal, which in air is oxidized to CdO. Since the ionic radius [17] of Cd(II) is much higher than that of  $Zn(II)$ , thus, based on the coulombic attraction the zinc will have a stronger  $M$ – $O<sub>I</sub>$  bond than that of cadmium. This would increase the energy needed to break the Zn–O bond, and thus increases the activation energy for the reaction. Dollimore and Griffths [18] also showed that, there is a decrease in the decomposition temperature with increase in the ionic radius of the metal ion. A decrease in the  $M-O<sub>I</sub>$  bond strength would thus lead to a decrease in the decomposition temperature. Thus, the  $CdC<sub>2</sub>O<sub>4</sub>$  will posses a lower decomposition temperature than  $ZnC_2O_4$  as can be observed from the DTA-TG curves (Fig. 1).

In addition, the thermal stability of the metal oxalates decrease with the increase in the electron affinity of the metal ion. The oxidation–reduction potential measures the relative electron affinities of the metal ions forming oxalates, since Dq values of  $H_2O$  is near to that of  $C_2O_4$ <sup>-</sup> [21]. The reduction potential of cadmium ( $E_{\text{Cd}^{2+}/\text{Cd}}^{0} = -0.403 \text{ V}$ ) is higher than that of zinc  $(E_{Zn^{2+}/Zn}^0 = -0.763 \text{ V})$ , therefore, the



Fig. 6. Plots of the activation energies versus  $\alpha$  calculated by Ozawa method for the thermal decomposition of CdC<sub>2</sub>O<sub>4</sub> and ZnC<sub>2</sub>O<sub>4</sub> in their mixture.

<span id="page-7-0"></span>thermal stability of  $CdC_2O_4$  is lower than that of  $ZnC_2O_4$ . The same effect was observed for central metal ions in potassium salts of metal oxalato complexes [21].

Moreover, the effect of the enthalpy of the reaction on the sample temperature and activation energy of the decomposition cannot be ignored [22,23]. The exothermicity of the  $CdC<sub>2</sub>O<sub>4</sub>$  decomposition is more than the  $ZnC<sub>2</sub>O<sub>4</sub>$  decomposition as evident from DTA curve (Fig. 1). This is due to the fact that the  $CdC<sub>2</sub>O<sub>4</sub>$  decomposition in air is accompanied by the exothermic oxidation reaction of cadmium metal to CdO. The excessive heat transfer would allow ease rupture of the M–O<sub>I</sub> bond in the CdC<sub>2</sub>O<sub>4</sub> than in the ZnC<sub>2</sub>O<sub>4</sub>.

# **4. Conclusions**

DTA-TG experiments of  $CdC_2O_4.3H_2O-ZnC_2O_4.2H_2O$ (1:1 mol ratio) mixture in air show that the mixture was completely decomposed to CdO–ZnO mixture through four well-defined steps. Intermediate decomposition products as well as the final products were characterized by X-ray diffraction and SEM techniques. XRD experiments show the absence of any formed solid solution even by raising the calcinations temperature to  $800\degree$ C. The increase in the intensity of the diffraction lines by raising the calcinations temperature from 400 to 800 $\degree$ C is attributed to the grain growth of the decomposition products. SEM experiments confirmed this result as the fine granules obtained at 400 ◦C were coalesced into large aggregates of large crystals when calcined at  $800\degree$ C. Kinetic analysis of the data for the oxalate decomposition steps according to the integral composite method showed that the oxalate decomposition steps are best described by the Avrami–Erofeev equation characteristic of the solid state nucleation growth mechanism. The activation parameters were then calculated and discussed in view of the ionic radius and the electronegativity of the metal ions.

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